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Kinetic Modeling of Cyclohexane and n-Propylcyclohexane Oxidation with the PAH Precursor Formation

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A reaction mechanism of cyclohexane ($\text{cyC}_6\text{H}_{12}$) and n-propylcyclohexane ($\text{cyC}_9\text{H}_{18}$) is developed to study its oxidation at both low and high temperatures, including PAH precursors routes. The cyclohexane oxidation kinetic mechanism is a significant update of the model developed earlier in DLR. The new $\text{cyC}_6\text{H}_{12}$ model is based on the most recent studied $\text{C}_0\text{-C}_3$ chemistry and includes the PAH sub-model up to 5-ringed molecules. Improvements have been done through the rivaling the main reaction classes, uncertainty boundaries of the rate coefficients and an inclusion of two additive low-temperature reaction pathways: cyclohexenyl peroxy formation, and isomerization of hydroperoxy peroxy radical. The $\text{cyC}_6\text{H}_{12}$ mechanism, successfully validated on the ignition delay data from rapid compression machines (RCM) and shock tube experiments, as well as laminar flame speed data and concentration profiles, model was then further extended to the n-propylcyclohexane oxidation model. For our knowledge, the low-temperature $\text{cyC}_9\text{H}_{18}$ oxidation scheme was earlier not presented in the literature. It is shown, that unlike $\text{cyC}_6\text{H}_{12}$ the low-temperature ignition of n-propylcyclohexane demonstrates negative temperature coefficient (NTC) behavior. The pathways towards production of benzene as the first aromatics was investigated under the different temperature regimes.

I. Introduction

PERFORMANCE and in particular emissions of any combustion devices are strongly dependent on the fuel and the underlying chemistry. Practical fuels such as kerosene are complex mixtures of several hundred individual species, which can be divided into four hydrocarbon families (n-/i-paraffins, naphthenes (cyclo-paraffins) and aromatics). Cycloalkanes (naphthenes) are an important chemical class of hydrocarbons found in diesel (up to 35%), kerosene (~20%) and gasoline (~10%), which affects the ignition quality of the fuel. Also cycloalkanes can raise soot emission levels because they are known to dehydrogenate and produce aromatics which can initiate the chain reaction for the production of polycyclic aromatics to soot formation and growth. Therefore, kinetic investigation of cyclohexane ($\text{cyC}_6\text{H}_{12}$) as the simplest naphthene molecule, and n-propylcyclohexane as the most convenient substituted naphthenes in the composition of commercial fuels (especially in jet surrogates) have a great importance in the way predicting the oxidation behavior of conventional fuels and pollution formation.

Despite of numerous investigations [1-21], up to now the published reaction models for $\text{cyC}_6\text{H}_{12}$ demonstrate significant discrepancies in the kinetic parameters and results. The uncertainty of reaction rate coefficients for some reaction classes are extremely high and can reach more than 1000. The ignition delay time measurements performed in the rapid compression machine (RCM) [11, 17] and in the shock tubes (ST) [16, 22] report contradictive information: NTC region observed for the $\text{cyC}_6\text{H}_{12}$ ignition in the RCM was not detected in the ST experiments.

The n-propylcyclohexane oxidation chemistry is sufficiently less investigated and based on the $\text{cyC}_6\text{H}_{12}$ model, consequently takes on every problems of the $\text{cyC}_6\text{H}_{12}$ modeling. Only few studies were published [3, 23, 24] concerning mostly high-temperature oxidation of the $\text{cyC}_9\text{H}_{18}$.

In the present paper, the earlier developed [25] $\text{cyC}_9\text{H}_{18}$ oxidation model was analyzed and is modified and further developed on the basis of the recently updated and extended $\text{cyC}_6\text{H}_{12}$ model [26]. The uncertainty of the key reaction types for both high- and low-temperature scheme have been evaluated. The required thermochemical properties

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specifically for low-temperature species, which have more complex structures, are revised and evaluated, applying Benson's additivity method with new available updates of Benson's groups [27] and ring corrections. The second focus of the paper is the analysis and comparison of the main reaction classes related to the cyclohexane ($\text{cyC}_6\text{H}_{12}$) and n-propylcyclohexane ($\text{cyC}_9\text{H}_{18}$) oxidation at lower temperature. This analysis was carried out using the recently published shock tube ignition delay data [22]. Due to the lack of adequate experimental data on species concentration profiles, relevant to n-propylcyclohexane combustion from burn stabilized flame, the routes to production of benzene (A1) as the first substituted aromatics were analyzed at simulation of the auto ignition data for fuel-rich ($\phi=2$) and atmospheric pressure conditions.

II. Kinetic Model

The current kinetic mechanism implies $\text{C}_0\text{-C}_2$ chemistry from the recent researches of Slavinskaya et al., [28, 29] the further improvements of the cyclohexane oxidation model developed by Abbasi et al. [26] and the n-propylcyclohexane reactions scheme established in Slavinskaya et al. [25].

The cyclohexane oxidation model of Abbasi et al. [26] were extended with two additive pathways: isomerization of $\text{cyOOC}_6\text{H}_{10}\text{OOH}$ through the internal hydrogen transfer yielding more stable $\text{cyC}_6\text{H}_9(\text{OOH})_2$ and the secondary low- temperature cyclohexene, $\text{cyC}_6\text{H}_{10}$, oxidation. The possible isomers of $\text{cyC}_6\text{H}_9(\text{OOH})_2$ were grouped in a single lumped component, which dissociates into cyclic ketohydroperoxide and OH. This step was included in the scheme to increase the concentrations of less reactive HO_2 and cyclohexanone radicals in the intermediate temperature zone.

Cyclohexenyl, cyC_6H_9 , produced from cyclohexene due to the cascading cyclohexane dehydrogenation, prolongs now the low-temperature cyclohexene oxidation after oxygen addition. This path is competitive with the low-temperature hexyl oxidation. The developed $\text{cyC}_6\text{H}_{12}$ model [26] satisfactorily reproduces the experimental data for ignition delay times, laminar flame speeds and concentration profiles measured in laminar flames. That makes it valuable for the application as a basic model in development of the kinetics schemes for larger and substituted naphthenes.

At the establishment of the sub-model for n-propylcyclohexane oxidation, it was assumed, that, main pathways are determined by its molecular structure and are the combination of the main reaction paths inherent in the cyclohexane and acyclic alkanes (nC_3H_7) oxidation, and has two regimes of oxidation, high- and low-temperature.

The n-propylcyclohexane high temperature oxidation proceeds through: unimolecular fuel decomposition; H-atom abstraction leading to cycloalkyl radicals, three isomers are consider , $\text{cyC}_9\text{H}_{17}\text{A}$, $\text{cyC}_9\text{H}_{17}\text{B}$, $\text{cyC}_9\text{H}_{17}\text{E}$; β -scission decomposition; cascading dehydrogenation leading to benzene and smaller radicals; isomerization and decomposition of linear radicals after the ring-opening step, Fig.1. The related rate constants were evaluated as analogous to those for the cyclohexane and propyl and linear alkane reactions.

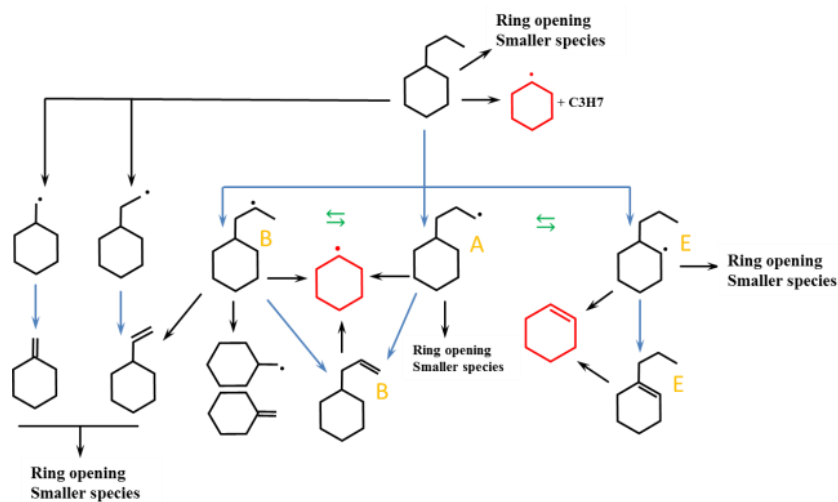


Figure 1. Principal scheme of the high temperature oxidation of $\text{cyC}_9\text{H}_{18}$.

For the low-temperature oxidation of n-propylcyclohexane due to the high uncertainties in reaction paths, reaction rate coefficients and reduced number of experimental data, only 7 main reaction paths have been adopted in the reaction mechanism. This our decision follows from the available information related to the low-temperature reactions

of the cycloalkanes. Table 1 collects the major evaluations/calculations performed for the rate coefficients of cyclohexane and methyl-cyclohexane low-temperature oxidation reactions. As it can be understood, the number of performed investigations is very limited and those related directly to n-propylcyclohexane are critical.

Table 1. Literature evaluations of the reaction coefficients for the low-temperature $\text{cyC}_6\text{H}_{12}$ oxidation

Ref.	$\text{R} + \text{O}_2 = \text{ROO}$	$\text{ROO} = \text{QOOH}$	$\text{ROO} = \text{Q} + \text{HO}_2$
Pitz et al. [30]	Analogous to n-alkanes	Analogous to n-alkanes, considering corrections in the number of internal rotors and structure of transient complexes.	
Cavalotti et al. [7]	Quantum chem. calculations (B3LYP/6-31g(d,p))	Quantum chem. calculations (B3LYP/6-31g(d,p))	Quantum chem. calculations (B3LYP/6-31g(d,p))
Silke et al. [8]	Analogous to n-alkanes, refers to Pitz et al. [30]	Analogous to n-alkanes with $\text{cyC}_6\text{H}_{12}$ isomerization correction from [30].	Reduced data of to Cavalotti et al. [7] with a factor of 2.
Sirjean et al. [6]		Quantum chem. calculations CBS-QB3 level.	

On the Figure 2, the finally included in the scheme isomers, and steps of the low-temperature n-propylcyclohexane conversion are demonstrated. These steps proceed through the largely accepted and employed kinetic schemes of the low-temperature alkane oxidation [31, 32] with the cyclo-specific and adopted isomer-specific modifications:

- 1) addition reaction with O_2 ;
- 2) isomerization of cyclic peroxy $\text{cyROO}\cdot$ to $\text{cyQOOH}\cdot$ hydroperoxy radical;
- 3) decomposition of $\text{cyQOOH}\cdot$ to cycloolefin and HO_2 ;
- 4) decomposition of cycloolefin;
- 5) O_2 addition to $\text{cyQOOH}\cdot$ with formation of $\text{O}_2\text{QOOH}\cdot$;
- 6) decomposition of $\text{O}_2\text{QOOH}\cdot$ to cyclic ketohydroperoxides;
- 7) Decomposition of ketohydroperoxides.

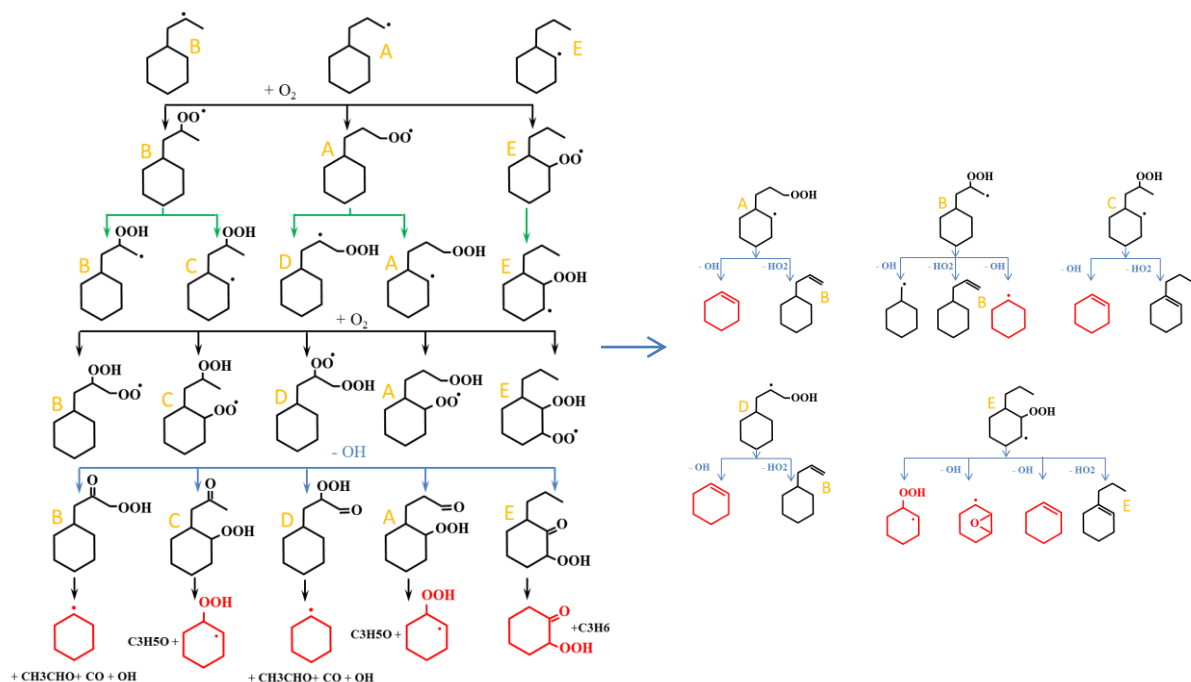


Figure 2. Principal scheme of the low temperature oxidation of $\text{cyC}_6\text{H}_{12}$.

Table 2. Thermodynamic properties of n-propylcyclohexane relevant sub-model species.

Species	$\Delta H_f^0 / \text{kJ}\cdot\text{mol}^{-1}$	$S^0 / \text{J}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$	$C_p(T) / \text{J}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$						
			300	400	500	600	800	1000	1500
cyC ₉ H ₁₈	-195.17	419.15	172.74	235.72	292.28	341.56	416.46	469.92	546.57
cyC ₉ H ₁₇ A	-3.73	431.54	171.91	233.19	287.57	334.59	405.61	456.07	527.98
cyC ₉ H ₁₇ B	-18.89	424.60	171.32	232.17	286.23	333.21	404.62	453.33	525.17
cyC ₉ H ₁₇ E	-18.92	424.59	171.35	232.22	286.29	333.29	404.98	455.30	527.65
cyC ₈ H ₁₅	-10.96	484.26	152.48	207.05	256.30	299.52	365.98	413.19	480.82
cyC ₈ H ₁₄	-48.76	372.66	138.32	192.10	239.98	281.48	344.11	387.78	449.58
cyC ₇ H ₁₃	37.13	346.94	126.17	175.07	218.63	256.39	313.34	352.88	408.91
cyC ₇ H ₁₂	-35.25	329.36	120.85	165.51	206.08	241.83	296.85	335.23	388.86
cyC ₉ H ₁₇ OOA	-138.99	483.18	188.79	253.36	311.34	361.76	437.84	491.51	577.42
cyC ₉ H ₁₇ OOB	-157.22	474.82	190.83	256.40	314.84	365.25	440.46	493.59	576.73
cyC ₉ H ₁₇ OOE	-157.22	474.82	190.83	256.40	314.84	365.25	440.46	493.59	576.73
cyC ₉ H ₁₆ OOHA	-97.54	503.37	203.33	267.84	323.33	371.04	444.45	494.11	570.71
cyC ₉ H ₁₆ OOHB	-80.70	498.25	210.55	274.72	329.90	377.10	448.49	495.48	567.87
cyC ₉ H ₁₆ OOHC	-115.77	495.01	205.37	270.89	326.82	374.52	447.07	496.19	570.03
cyC ₉ H ₁₆ OOHD	-96.05	505.29	200.74	264.91	320.20	367.84	441.87	494.69	568.21
cyC ₉ H ₁₆ OOHE	-96.41	491.32	209.98	273.67	328.58	375.72	447.51	494.63	567.46
cyC ₉ H ₁₆ OE	-218.83	434.53	205.93	275.69	336.17	387.30	462.28	518.58	580.60
cyOOC ₉ H ₁₆ OOHA	-235.84	553.60	222.80	292.03	351.87	402.99	479.93	532.42	619.66
cyOOC ₉ H ₁₆ OOHB	-235.84	553.60	222.80	292.03	351.87	402.99	479.93	532.42	619.66
cyOOC ₉ H ₁₆ OOHC	-274.24	584.65	247.72	324.17	389.86	445.61	528.87	588.33	657.84
cyOOC ₉ H ₁₆ OOHD	-235.84	553.60	222.80	292.03	351.87	402.99	479.93	532.42	619.66
cyOOC ₉ H ₁₆ OOHE	-274.24	584.65	247.72	324.17	389.86	445.61	528.87	588.33	657.84
cyOC ₉ H ₁₅ OOHA	-375.25	509.30	213.43	277.95	332.61	379.22	450.84	499.24	574.20
cyOC ₉ H ₁₅ OOHB	-375.65	511.84	215.09	282.19	337.69	384.42	456.01	503.66	577.08
cyOC ₉ H ₁₅ OOHC	-404.91	513.76	210.10	274.91	329.81	376.78	449.55	498.85	577.74
cyOC ₉ H ₁₅ OOHD	-375.25	509.30	213.43	277.95	332.61	379.22	450.84	499.24	574.20
cyOC ₉ H ₁₅ OOHE	-404.37	514.01	217.03	281.44	333.30	377.42	449.29	497.64	570.73
cyC ₉ H ₁₆ B	-70.44	412.11	161.21	221.08	274.30	320.42	390.21	439.42	509.19
cyC ₉ H ₁₆ E	-73.35	422.33	168.85	226.90	277.05	319.80	384.29	431.47	495.02

The reaction rates of peroxy radicals, ROO and OOQOOH, following from analogues with acyclic alkanes applying cyclo-specific rate modification rules studied intensively in [9, 30] and from recommendations collected in the Table1.

Thermodynamic properties for several cyclic species were newly estimated and revised based on Benson's additivity approach including cyclic and bicyclic ring correction groups, reported in [27], Table 2. For that, properties of some new Benson's groups were estimated, Table 3.

Table 3. The calculated thermodynamic values for new groups.

No.	Group	ΔH_f^0 kJ·mol ⁻¹	S^0 J·mol ⁻¹ ·K ⁻¹	$C_p(T, K) / J \cdot mol^{-1} \cdot K^{-1}$						
				300	400	500	600	800	1000	1500
G1	C-(C•)(C)(O)(H)	-10.77	-49.75	24.63	30.87	35.06	38.28	41.67	42.00	47.20
G2	C•-(O)(H) ₂	142.50	127.10	26.19	29.00	32.90	36.16	39.90	44.04	50.15
G3	C•-(C)(O)(H)	134.68	41.09	15.76	19.00	23.41	27.10	30.58	32.07	34.66
G4	CO-(Cd)(C)	-146.52	52.20	24.72	29.61	34.06	37.86	41.10	42.36	45.75
G5	C•-(CO)(H) ₂	140.44	126.21	23.82	28.55	32.60	36.08	40.40	44.06	47.91
G6	C•-(Cd) ₂ (H)	81.19	25.46	16.60	24.20	30.87	35.66	40.85	45.86	50.07
G7	C•-(C)(Cd)(O)	84.01	-68.99	11.28	15.32	19.97	23.24	24.86	25.52	26.06
G8	CO-(C)(H)	-123.81	137.04	29.60	33.23	37.20	41.00	46.63	50.80	56.00
G9	CO-(C•)(H)	-115.24	141.92	31.31	34.83	38.37	41.72	48.73	53.61	62.35
G10	O-(C•)(O)	-11.51	32.92	15.40	19.63	22.25	24.71	29.69	30.80	34.62

The non-linear least squares method and its numeric realization FUMILI [33] has been applied to estimate the upper f_u and lower f_l uncertainty factors for the main reactions:

$$\text{Eq.(1)} \quad f_u(T) = \log \left[\frac{k_{upper}(T)}{k_0(T)} \right], f_l(T) = \log \left[\frac{k_0(T)}{k_{low}(T)} \right]$$

The in house developed tool, named as “Reac-UQ”, was used for the mean of quantification of uncertainty intervals. Fig.3 represents an example of uncertainty analysis for some reactions of high temperature regime.

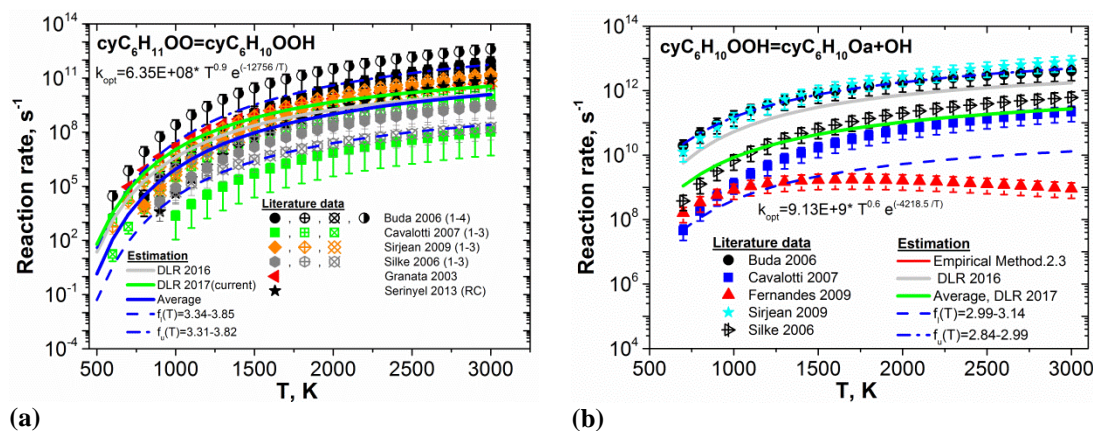


Figure 3. Uncertainty estimation and analysis of reaction rate vs. temperature, based on the available literature data [9, 7, 34, 8, 35, 4]. (a): numbers in parenthesis count isomers studied in the papers.

The uncertainty factors evaluated for the reactions analysed on the Fig.3, are equal approximately 3-4. The same value were prescribed to the rate coefficients of the n-propylcyclohexane oxidation reaction scheme. Due to the lack of data, it is not able to perform such analysis for cyC_9H_{18} .

III. Results and discussion

The behaviour of the low-temperature cyclohexane and n-propylcyclohexane oxidation models were validated on ignition delay times from rapid compression machines (RCM) [11, 17, 24] and shock tubes experiments (ST) [36] [23, 22], over the wide temperature range of 600-1700K at various equivalence ratios and pressure ranges.

Figure 4 demonstrates the comparison of the simulated ignition delay times and observed in shock tube [22] under approximatively identical conditions for cyclohexane, Fig. 4a,b, and n-propylcyclohexane, Fig. 4c,d. The simulations and experiments agree well and clearly indicate, that the ignition delay time shape for cyclohexane does not have the negative temperature coefficient, Fig. 4b, while the shape for n-propylcyclohexane demonstrates light NTC behavior, Fig. 4d.

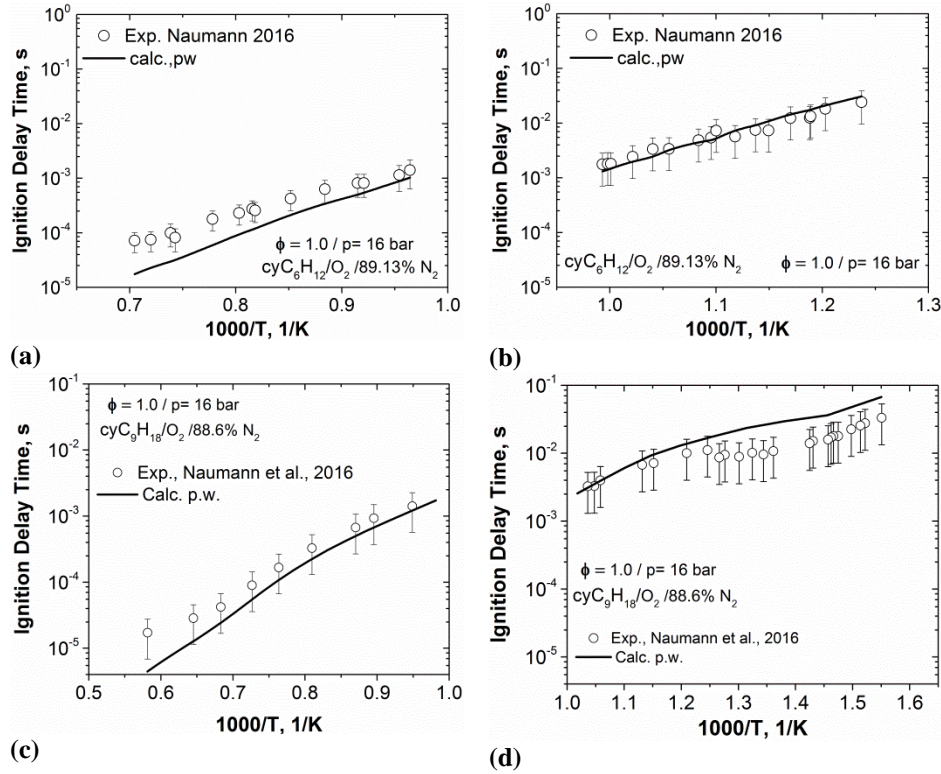


Figure 4. Comparison of simulated ignition delay times with the ST experiments [22] for stoichiometric mixtures: a),b) cyclohexane; c),d) n-propylcyclohexane.

We analyzed the behavior of the OH and temperature profiles for both fuels, Fig. 5. It can be clearly see, that unlike $\text{cyC}_6\text{H}_{12}$, $\text{cyC}_9\text{H}_{18}$ has peaks on the OH profile, which correspond to the cool flame and the two stage ignition.

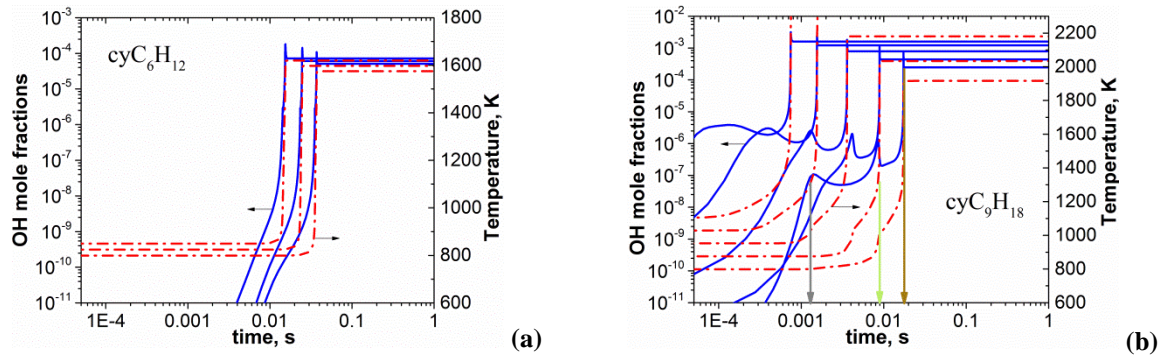


Figure 5. OH concentrations and T profiles versus time, for $T_s=800-1100\text{K}$, $P_s=16\text{bar}$: a) cyclohexane; b) n-propylcyclohexane.

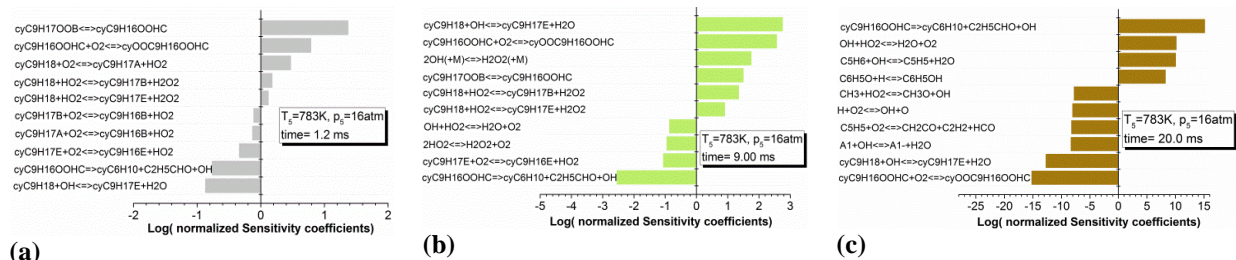


Figure 6. Normalized sensitivity coefficients of ignition delay times to reactions calculated for the time points marked on the Fig.5b.

How it follows from the rate of production analysis, the first peaks on the OH concentration profiles are mostly produced in reaction sequences, which are started with the oxygen addition to the cyC₉H₁₇A and cyC₉H₁₇B, Fig.2. The radical cyC₉H₁₇E yields in the OH production with temperature growth. Hereby the peroxy and hydroperoxy radicals, mostly cyC₉H₁₇OOB, produced on the substituent group, control the low-temperature oxidation of the cyC₉H₁₈ on the first stages of the chain reaction development. The process evolution is well highlighted with the results of sensitivity analysis performed for three time points, correspond to the OH and T arise, marked on the Fig.5. Reactions of the substituted groups control the chain-branching process for the time region of the first and second peaks on the OH concentration profile, Fig.6a,b. With a temperature increase reactions of cyC₉H₁₇OOB become important, Fig.6b,c. Just after ignition, reactions of the aromatic molecules dominate.

One can conclude, that reactions of the substituted groups cause the NTC behavior at the low-temperature oxidation of cyC₉H₁₈. Cyclic peroxy radicals are less reactive, therefore cyclohexane has the gradient change, an acceleration of the overall reaction rate, instead the NTC for intermediate temperatures, Fig. 4a and 4b.

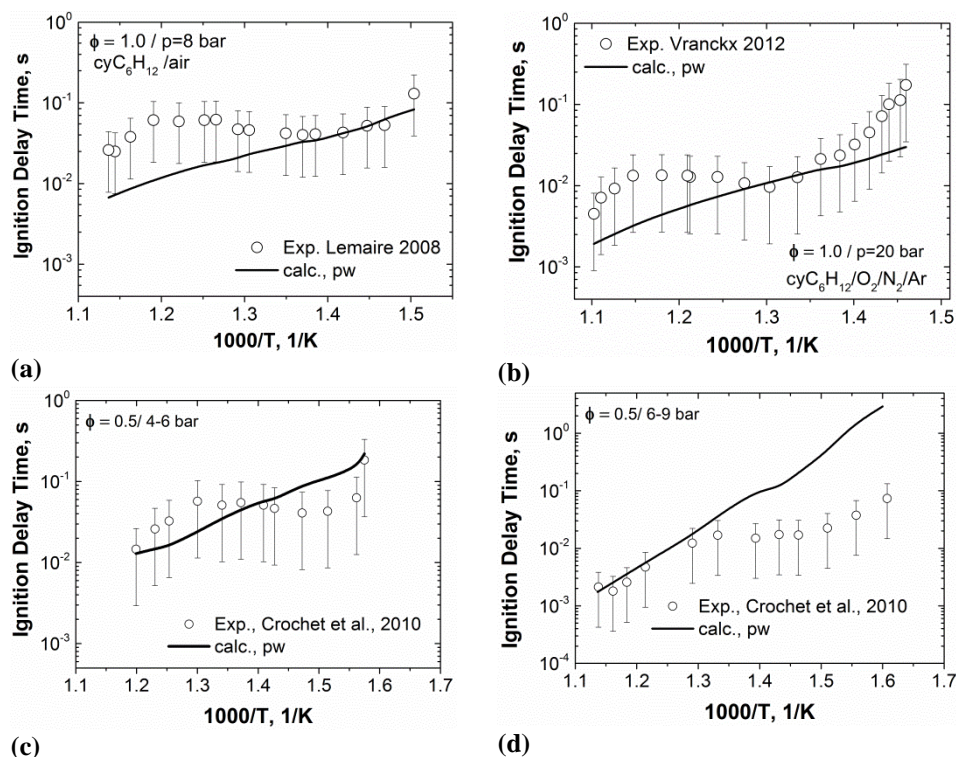


Figure 7. Comparison of simulated ignition delay times with the RCM experiments [11, 17, 24] for: a),b) cyclohexane; c),d) n-propylcyclohexane.

Table 4. Adopted reaction rate coefficients.

Reaction path	Isomers	A	n	Ea/cal	Note*
$R+O_2=RO_2$	A,B	$5.00E+19$	-2.5	0.0	a
	E	$1.00E+19$	-2.5	0.0	a
$RO_2=QOOH$	A→D	$0.50e+12$	0.0	29300	b
	A→A	$2.00e+12$	0.0	24045	b
	B→B	$0.50e+12$	0.0	29300	b
	B→C	$2.00e+12$	0.0	24045	b
	E→E	$2.00e+12$	0.0	24045	b
$cyQOOH=cy\text{-Olefin}+Aldehyde+OH$	A,C,D	$1.20E+15$	0.0	22500	c
$cyQOOH=cy\text{-Alkyl}+Keton\ rad.+OH$	B,D	$1.00E+17$	0.0	35000	d
$cyQOOH=cy\text{-Olefin}+HO_2$	A-E	$1.21E+13$	-0.59	30800	e
$cyQOOH=cyQ'OOH+Olefin$	E	$2.5E+18$	-0.19	30350	e
$cyQOOH=expoxies+OH$	E	$8.00E+13$	0.0	25400	f
$cyQOOH+O_2=cyOOQOOH$	A-E	$0.50E+20$	-2.5	0.0	g
$cyOOQOOH=cy\text{-Ketohydroperoxy}+OH$	A-E	$2.00e+12$	0.00	24045	f
$cy\text{-Ketohydroperoxy decomposition}$	A-E	$3.30E+16$	0.00	21000	h

*Note: a: modified by analogy with cyclohexane; b: isomerization on internal H-transfer on secondary C-atom [37]; c: analogous to iC8 [38] ; e: analogous to n-alkanes [32, 38] f: isomerization H-transfer $ROO=QOOH$; g: analogous to O_2 addition h: analogous to n-C7 [32].

Generally, the NTC region was fixed in the RCM measurements for both, cyC_6H_{12} and cyC_9H_{18} , Fig.7. The cyC_6H_{12} model did not reproduce the two stage ignition with NTC behavior, but again an acceleration of the overall reaction rate, wherein simulations lie in the uncertainty boundaries of the measured data [11, 17], Fig.7a,b. The cyC_9H_{18} model demonstrates very weak trend to the NTC regime at the calculations, Fig.7c,d.

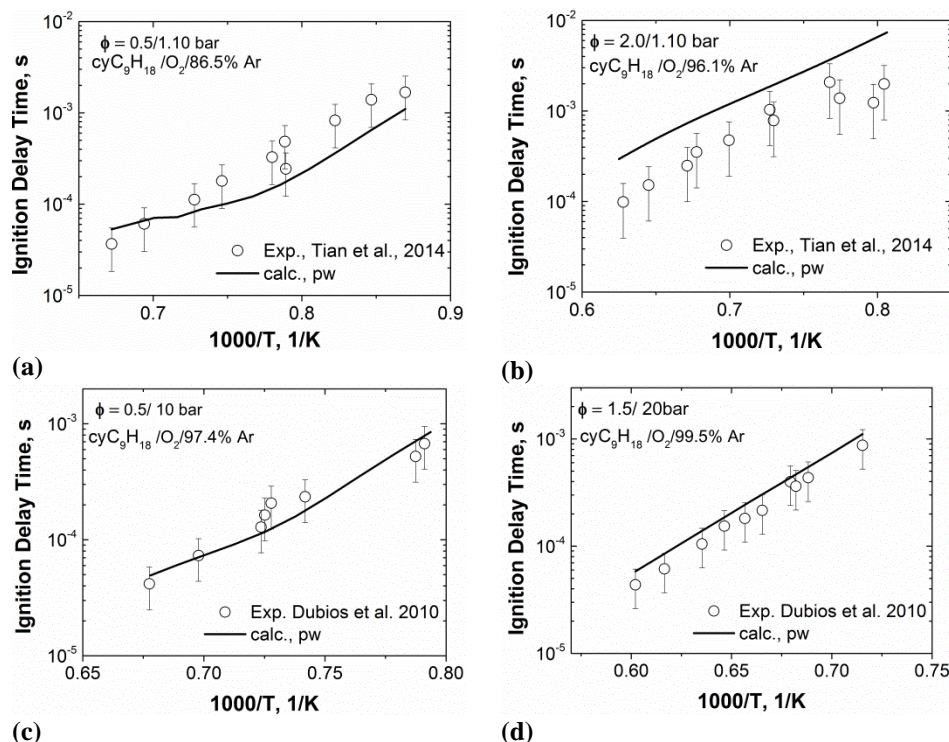


Figure 8. Comparison of simulated ignition delay times with ST experiments [36, 23] for: n-propylcyclohexane.

The simulations of data [24] lie in the uncertainty boundaries of measurements, Fig.6c, performed for the pressure 4-6 bar and temperature 600-900K. For the similar mixture and temperature range, but for the pressure 6-9 bar, the model overpredicts the experimental data at temperature 600-770K with a factor of 10. We assume, that this

discrepancy follows from the larger uncertainties of data measured in the rapid compression machines compared to those from shock tubes. These larger uncertainties are an accumulated effect of different well-known factors: the possible reactions in RCM during the compression stroke, heat losses, etc. On this way, for the final $\text{cyC}_9\text{H}_{18}$ model optimization and improvement only shock tube experiments were used. In the Table 4, the obtained reaction rate coefficients for the reactions of the low-temperature $\text{cyC}_9\text{H}_{18}$ oxidation are collected.

Figure 8 demonstrates further model validation on the shock tube data [36, 23]. Generally the model has good agreement with the experimental data, but overpredicts data for rich mixture [23], Fig.8b.

Due to the lack of adequate experimental data on species concentration profiles, relevant to the n-propylcyclohexane combustion from burn stabilized flame, the auto ignition data from shock tube of Tian et al. [23], measure in fuel-rich condition ($\phi=2$), atmospheric pressure, was utilized to investigate the routes to production of benzene (A1). Figure 9 demonstrates the analysis of the benzene rate of production carried out for time points before and after ignition. Before the ignition takes place ($T < 1500$ K), the fuel dissociation and dehydrogenation reactions are the controlling processes for the production of A1, Figure 9a. With temperature increase the production of A1 is mainly influenced by the interactions of small species, specifically PAH precursors, such as propargyl radical, $i\text{-C}_4\text{H}_5$, C_4H_6 . But in the post-ignition zone, at high temperatures, equilibrium of small radical reactions are shifted to the benzene decomposition, Figure 9b, and only dehydrogenation of fuel yields further in the A1 production.

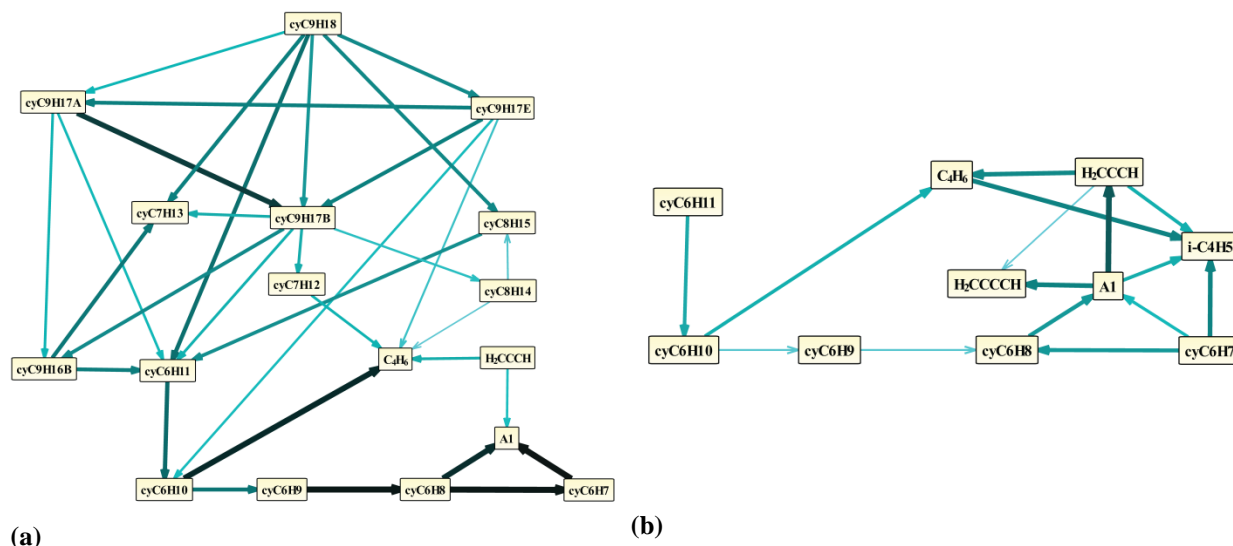


Figure 9. Benzene rate of production analysis performed at two different time intervals: a) before ignition b) after ignition. Analysis were carried with the aid of Chemical work Bench software [39].

IV. Conclusions

A semi-detailed reaction mechanism for low- and high-temperature cyclohexane and n-propylcyclohexane oxidation with PAH formation is developed. This mechanism is an improved extension of the cycloalkane oxidation sub-models of DLR hydrocarbon reaction database. In this modified extension, certain number of reaction paths were revised and optimized as the result of uncertainty and sensitivity analyses. It implements a new optimized syngas and acetylene sub model for $\text{C}_0\text{-C}_2$ chemistry. Special care has been taken to revise of rate parameters specific to cyclic alkanes and to evaluation of uncertainty intervals for the rate coefficients of most important reactions. This analysis revealed that actual uncertainty level of reaction rate coefficients is about 3.5. The low-temperature oxidation pathway of n-propylcyclohexane is developed only with the 7 key paths due to a lack of experimental and thermochemical data available for the n-propylcyclohexane chemistry. The adopted rate coefficients were evaluated with analogous to the acyclic alkanes with the cyclic-specific corrections. The thermodynamical properties of some molecules and radicals were newly calculated with group additivity rule.

The ignition simulations, thermochemistry, flow-rate and sensitivity analyses shown, that unlike cyclohexane, n-propylcyclohexane ignition has the NTC region, which is occurred at $800 < T < 1100$ K as a response to an increase of overall reactivity initiated by the chain branching reactions of peroxy- and hydroperoxy-radicals produced with substituted group of $\text{cyC}_9\text{H}_{18}$. Our numerical simulations are in accordance with the shock tube observations and

support this conclusion. Species rate of production were also performed to investigate the influential pathways to formation of the first aromatic ring. It has been seen that under the lower temperature regime production of A1 is mostly ruled by dehydrogenation of the fuel, however in higher temperatures it is mostly controlled by the smaller PAH precursors.

Further investigation of this matter would be very useful for the development of kinetic mechanisms for larger substituted naphthenes.

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